Amendments to the Claims:

This listing of claims will replace all prior versions and listings of claims in the application:

Listing of Claims:

Claims 1-24 (cancelled)

25. (currently amended) A ~~Microcrystalline~~ microcrystalline paraffin, prepared by ~~a ß-zeolite based catalytic hydroisomerization of~~ hydroisomerizing FT (Fischer-Tropsch) paraffins having a carbon chain length distribution in the range from 20 to 105, at temperatures above 200°C, by processing the FT paraffins with a catalyst based on a beta zeolite, the catalyst comprising 60 to 95 by mass of zeolite of the beta type, based on the combination of all components fired at 800°C, 5 to 39.8 by mass of gamma-aluminum oxide having a specific surface area of 150-350 m^2/g, calculated as Al_2O_3 and based on the combination of all components fired at 800°C, and one or more metals of transition group 8 of the periodic table, in an amount of 0.2 to 2.0 by mass, based on the combination of all components fired at 800°C, the one or more transition group 8 metals being attached to the gamma-aluminum oxide.

26. (currently amended) The ~~Microcrystalline~~ microcrystalline paraffin according to claim 25, wherein, at 25°C the paraffin is not liquid but at least paste-like to solid with a needle penetration value of less than 100 x 10^{-1} mm, measured in accordance with DIN 51579.

27. (currently amended) The ~~Microcrystalline~~ microcrystalline paraffin according to claim 25, wherein the paraffin is free of aromatic and heterocyclic compounds.

28. (currently amended) The ~~Microcrystalline~~ microcrystalline paraffin according to claim 25, wherein the paraffin is free of naphthenes.

29. (currently amended) The ~~Microcrystalline~~ microcrystalline paraffin according to claim 25, having a proportion by weight of isoalkanes that is greater than that of n-alkanes in the paraffin.

30. (cancelled)

31. (currently amended) Process for preparing a microcrystalline paraffin ~~according to claim 25,~~ by catalytic hydroisomerization ~~by steps of:~~ comprising

~~A. use of~~ processing FT (Fischer-Tropsch) paraffins, as a starting material, having carbon atoms in the range from 20 to 105; ~~and~~

~~B. use of~~ in the presence of a catalyst based on a ß-zeolite;

~~C. use of a process temperature above 200°C; and~~ wherein the process is conducted at a temperature above 200°C, and

~~D. action of pressure~~ at a pressure in a range of 2 to 20 MPa in the presence of hydrogen; wherein the catalyst comprises 60 to 95 by mass of zeolite of the beta type, based on the combination of all components fired at 800°C, 5 to 39.8 by mass of gamma-aluminum oxide having a specific surface area of 150-350 m^2/g, calculated as Al_2O_3 and based on the combination of all components fired at 800°C, and one or more metals of transition group 8 of the periodic table, in an amount of 0.2 to 2.0 by mass, based on the combination of all components fired at 800°C, the one or more transition group 8 metals being attached to the gamma-aluminum oxide.

32. (currently amended) Process according to claim 31, wherein the ß-zeolite~~, has~~ further comprises pores comprising a pore size between 0.50 and 0.80 nm ~~as support material and a metal of transition group 8 as active component~~.

33. (cancelled)

34. (cancelled)

35. (cancelled)

36. (currently amended) Process according to claim [[33,]] 31, wherein the pressure is 3 to 8 Mpa.

37. (currently amended) Process according to claim [[33,]] 31, wherein the ~~elevated temperature is a~~ process is conducted at a temperature of 230 to 270°C.

38. (currently amended) Process according to claim 31, ~~comprising a step of feeding~~ wherein the hydrogen is fed to the paraffin, ~~characterized by~~ in a feed ratio of hydrogen to FT paraffin from 100:1 to 2000:1 standard m^3 per m^3.

39. (currently amended) Process according to claim 31, ~~comprising a step of feeding~~ wherein the hydrogen is fed to the paraffin, ~~characterized by~~ in a feed ratio of hydrogen to FT paraffin from 250:1 to 600:1 standard m^3 per m^3.

40. (previously presented) Process according claim 31, wherein the process is carried out at a loading from 0.1 to 2.0 v/vh.

41. (currently amended) Process according to claim [[33,]] 32, wherein the catalyst has a pore size between 0.55 to 0.76 nm.

42. (cancelled)

43. (currently amended) Process according to claim [[42,]] 31, wherein the ~~catalyst~~ one or more metals of transition group 8 of the Periodic Table comprises platinum ~~as hydrogenation metal~~.

44. (previously presented) Process according to claim 43, wherein the platinum content of the catalyst is 0.1 to 2.0% by mass, based on a catalyst fired at 800°C.

45. (currently amended) Process according to claim 31, wherein the FT paraffins have a solidification point ~~range~~ ranging from 70 to 105°C.

46. (currently amended) Process according to claim 31, wherein the microcrystalline ~~paraffins are~~ paraffin is prepared from the FT paraffins in a single process step, ~~optionally additionally with removal of the short chain constituents~~.

Claims 47-50 (cancelled)

51. (previously presented) Process according claim 31, wherein the process is carried out at a loading from 0.2 to 0.8 v/vh.

52. (previously presented) Process according to claim 43, wherein the platinum content of the catalyst is 0.4 to 1.0% by mass, based on a catalyst fired at 800°C.

53. (previously presented) Process according to claim 45, wherein the FT paraffins have solidification points of 70, 80, 95 or 105°C.

54. (new) Process according to claim 46, wherein the microcrystalline paraffins are prepared from the FT paraffins in a single process step, with removal of the short chain constituents.